What is claimed is:

1. A process for producing low pour point hydrocarbon products having an initial boiling point above about 150 degrees C from a Fischer-Tropsch plant which comprises:

(a) recovering a feedstock comprising C_5 plus syncrude from a Fischer-Tropsch plant;

(b) dewaxing the C_5 plus syncrude feedstock in a catalytic dewaxing zone by contacting the C_5 plus syncrude feedstock with a dewaxing catalyst under dewaxing conditions, whereby a C_5 plus intermediate is produced having a lowered pour point relative to the C_5 plus syncrude feedstock;

(c) hydrofinishing the C_5 plus intermediate in a hydrofinishing zone under hydrofinishing conditions, whereby a UV stabilized C_5 plus product is produced; and

(d) separately collecting from the UV stabilized C_5 plus product a low pour point hydrocarbon product having an initial boiling point above about 150 degrees C.

2. The process of claim 1 wherein a low pour point diesel and a lubricating base oil are separately recovered from the UV stabilized C_5 plus product.

3. The process of claim 1 wherein the dewaxing catalyst of step (b) contains at least one active metal having hydrogenation activity.

4. The process of claim 3 wherein the dewaxing catalyst comprises an intermediate pore size SAPO.

5. The process of claim 4 wherein the dewaxing catalyst comprises at least one SAPO selected from the group consisting of SAPO-11, SAPO-31, and SAPO-41.

6. The process of claim 5 wherein the dewaxing catalyst comprises SAPO-11.

7. The process of claim 3 wherein the dewaxing catalyst comprises an intermediate pore size zeolite.

8. The process of claim 7 wherein the dewaxing catalyst comprises at least one zeolite selected from the group consisting of SSZ-32, ZSM-22, ZSM-23, ZSM-35, and ZSM-48.

9. The process of claim 8 wherein an ultra high VI, low pour point lubricating base oil is collected in step (d).

10. The process of claim 3 wherein at least one of the active metals is selected from the group consisting of platinum and palladium.

11. The process of claim 10 wherein at least one of the active metals is platinum.

12. The process of claim 3 wherein the dewaxing catalyst is a non-zeolitic molecular sieve and the active metal is added by non-aqueous addition.

13. The process of claim 1 wherein the hydrofinishing conditions of step (c) comprise a pressure of between about 200 psig to about 3000 psig.

14. The process of claim 13 wherein the hydrofinishing conditions comprise a pressure of between about 500 psig and about 2000 psig.

15. A process for producing low pour point syncrude products having an initial boiling point above about 120 degrees C from a Fischer-Tropsch plant which comprises:

(a) *recovering a feedstock comprising* C_5 *plus syncrude from a* Fischer-Tropsch plant;

(b) dewaxing the C_5 plus hydrocarbon feedstock in a hydroisomerization zone by contacting the C_5 plus syncrude feedstock with a hydroisomerization catalyst under hydroisomerization conditions, whereby an isomerized C_5 plus intermediate is produced having a lowered pour point relative to the C_5 plus syncrude feedstock;

(c) hydrofinishing the isomerized C_5 plus intermediate in a hydrofinishing zone under hydrofinishing conditions, whereby a UV stabilized C_5 plus product is produced; and

(d) separately collecting from the UV stabilized C_5 plus product a low pour point diesel product and a lubricating base oil product.

16. The process of claim 15 wherein the hydroisomerization catalyst comprises an intermediate pore size SAPO and at least one hydrogenation component comprising an active metal having hydrogenation activity.

17. The process of claim 16 wherein the hydroisomerization catalyst comprises at least one SAPO selected from the group consisting of SAPO-11, SAPO-31, and SAPO-41.

18. The process of claim 17 wherein the hydroisomerization catalyst comprises SAPO-11.

19. The process of claim 16 wherein at least one of the active metal is selected from the group consisting of platinum and palladium.

20. The process of claim 19 wherein at least one of the active metal is platinum.

21. The process of claim 16 wherein the active metal is added to the hydroisomerization catalyst by non-aqueous addition.

22. The process of claim 15 wherein the hydrofinishing conditions of step (c) comprise a pressure of between about 200 psig to about 3000 psig.

23. The process of claim 22 wherein the hydrofinishing conditions comprise a pressure of between about 500 psig and about 2000 psig.

24. The process of claim 16 wherein the cut-point for the separation of the low pour point diesel product from the lubricating base oil product is pre-selected to maximize the yield of the low pour point diesel product.

25. A process for producing ultra high VI, low pour point lubricating base oil product from a Fischer-Tropsch plant which comprises:

(a) recovering a feedstock comprising C_5 plus syncrude from a Fischer-Tropsch plant;

(b) dewaxing the C_5 plus syncrude feedstock in a catalytic hydrodewaxing zone by contacting the C_5 plus hydrocarbon feedstock with hydroisomerization dewaxing catalyst comprising an intermediate pore size zeolite and at least one metal having hydrogenation activity, said dewaxing being carried out under hydrodewaxing conditions selected to produce an C_5 plus intermediate having a lowered pour point relative to the C_5 plus syncrude feedstock;

(c) hydrofinishing the C_5 plus intermediate in a hydrofinishing zone under hydrofinishing conditions, whereby a UV stabilized C_5 plus product is produced; and

(d) separately collecting from the UV stabilized C_5 plus product an ultra high VI, low pour point lubricating base oil product.

26. The process of claim 25 wherein the intermediate pore size zeolite is also characterized by having one-dimensional pores one-dimensional pores.

27. The process of claim 25 wherein the intermediate pore size zeolite having one dimensional pores comprises at least one zeolite selected from the group consisting of SSZ-32, ZSM-22, and ZSM-23.

28. The process of claim 25 wherein at least one of the active metal is selected from the group consisting of platinum and palladium.

29. The process of claim 28 wherein at least one of the active metal is platinum.

30. The process of claim 25 wherein the hydrofinishing conditions of step (c) comprise a pressure of between about 200 psig to about 3000 psig.

31. The process of claim 30 wherein the hydrofinishing conditions comprise a pressure of between about 500 psig and about 2000 psig.